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(21) International Application Number: PCT/NL94/00242 (22) International Filing Date: 5 October 1994 (05.10.94) (30) Priority Data: 9301067 11 October 1993 (11.10.93) BE (71) Applicant (for all designated States except US): DSM N.V. [NL/NL]; Het Overloon 1, NL-6411 TE Heerlen (NL). (72) Inventors; and (75) Inventors/Applicants (for US only): VAN DOREMAELE, Gerardus, Henricus, Josephus [NL/NL]; Op de Hoef 6, NL-6132 HN Sittard (NL). VAN BEEK, Johannes, Antonius, Josephus [NL/NL]; St. Servaasbolwerk 10, NL-6211 NB Maastricht (NL). POSTEMA, Rutgerus, Antonie, Jacobus [NL/NL]; Salmstraat 48, NL-6161 EN Geleen (NL). (74) Agent: NIEUWKAMP, Johannes, Gerardus, Maria; Octrooi-bureau DSM, P.O. Box 9, NL-6160 MA Geleen (NL).		(81) Designated States: AM, AU, BB, BG, BR, BY, CA, CN, CZ, EE, FI, GE, HU, JP, KG, KP, KR, KZ, LK, LR, LT, LV, MD, MG, MN, NO, NZ, PL, RO, RU, SI, SK, TJ, TT, UA, US, UZ, VN, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG), ARIPO patent (KE, MW, SD, SZ). Published <i>With international search report.</i>
(54) Title: PROCESS FOR THE POLYMERIZATION OF AN OLEFIN IN THE PRESENCE OF A CATALYST SYSTEM COMPRISING A HALOGEN METALLOCENE (57) Abstract A process for the polymerization of an olefin in the presence of a catalyst system composed of: a) a halogen metallocene, b) a co-catalyst which forms a stable anion, c) an aluminium-containing alkylating agent, with the aluminium-containing alkylating agent is a mixture or reaction product of an alkyl aluminium compound and an alcohol.		

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5 PROCESS FOR THE POLYMERIZATION OF AN OLEFIN
 IN THE PRESENCE OF A CATALYST SYSTEM COMPRISING
 A HALOGEN METALLOCENE

 The invention relates to a process for the
10 polymerization of an olefin in the presence of a catalyst
system comprising a halogen metallocene.

 It is known that metallocene compounds are
active as a catalyst component in the polymerization of
olefin(s). They offer high activity in such a
15 polymerization of olefins, provided that they are used in
combination with a second catalyst component, hereinafter
referred to as co-catalyst. The combination of a
metallocene compound with a linear or cyclic aluminoxane
as a co-catalyst is known from EP-A-69,951. The
20 combination of a metallocene compound and aluminoxane has
also been described in many other publications. A
disadvantage of using aluminoxanes as co-catalysts is that
it is necessary to employ a large quantity of co-catalyst
relative to the metallocene compound. This generally leads
25 to a high residual aluminium content in the product of the
polymerization, the polyolefin.

 It is also known, for example from EP-A-468,537,
to employ a compound forming a stable anion as a co-
catalyst beside a metallocene catalyst. An example of a
30 suitably stable anion is tetrakis(pentafluorophenyl)-
borate. A catalyst system incorporating a co-catalyst that
forms a stable anion is referred to as an ionic catalyst
system. Ionic systems have the advantage that no large
quantities of aluminoxanes need to be used as co-catalyst.
35 Ionic metallocene systems are described in many
publications, for example in WO91/09882, WO91/12285 and
WO92/05208, to which the reader is referred.

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A drawback of ionic catalyst systems is that the metallocene compound from which the catalyst is formed must be a metallocene dialkyl compound. Metallocene dialkyl compounds are difficult to maintain since they decompose easily. For this reason, the required metallocene dialkyl compound is usually prepared immediately before the polymerization by alkylating a halogen metallocene with an alkylating agent such as methyllithium or a methyl Grignard reagent. A method for preparing a stable catalyst starting from a halogen metallocene is known from EP-A-500,944. The latter contains a description, amongst other things, of catalysts obtained from:

- a) a halogen metallocene
 - b) a co-catalyst which can form a stable anion under polymerization conditions and
 - c) an aluminium-containing alkylating agent.
- Some activity is found when an olefin is polymerized without using aluminoxane. However, the activity is not high enough. Moreover, it is necessary to add a large amount of aluminium-containing alkylating agent. The sequence of addition of the components started from is also critical. See, for example, Comparative Example 3 of EP-A-500,944. In addition, trimethylaluminium cannot be used as an alkylating agent (see Example 1 from EP-A-500,944).

The object of the invention is to provide a metallocene catalyst system for olefin polymerization with a high activity, the said catalyst system resulting in a polymer with a low residual aluminium content. The invention also relates to a simple method for preparing the catalyst from stable components.

According to the invention this object is achieved through the polymerization of an olefin in the presence of a catalyst system comprising:

- a) a halogen metallocene
- b) a co-catalyst which can form a stable anion under

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polymerization conditions and
c) an aluminium-containing alkylating agent,
characterised in that the aluminium-containing alkylating
agent is a mixture or reaction product of an alkyl
5 aluminium compound and an alcohol.

According to the invention, it is possible to
obtain higher polymerization activity than by using the
process described in EP-A-500,944. The quantity of
aluminium-containing alkylating agent that must be added
10 is considerably smaller than when the process in EP-A-
500,944 is employed. Furthermore it has proved to be
possible to use trimethylaluminium as an alkylating agent.
In addition the sequence of addition of the co-catalyst,
halogen metallocene and aluminium-containing alkylating
15 agent is less critical than in the process described in
EP-A-500,944. The polyolefins which are prepared have a
low residual catalyst content, including a low residual
aluminium content.

According to the invention, "halogen
20 metallocene" means a coordination compound of a metal from
group 4, 5 or 6 of the Periodic Table of the Elements and
having at least one halogen atom attached to the metal,
with the coordination compound containing one or more
substituted or unsubstituted η_5 -cyclopentadienyl groups.
25 The Periodic Table of the Elements is understood to be the
IUPAC version (New Notation), as printed on the jacket of
the Handbook of Chemistry and Physics, 70th edition, CRC
Press, 1989-1990. According to the invention, " η_5 -
cyclopentadienyl groups" is understood to include
30 fluorenyl or indenyl groups.

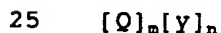
The η_5 -cyclopentadienyl groups in the
coordination compound can be the same or different.

The following abbreviations are used: Cp for a
cyclopentadienyl group, Ind for an indenyl group and Flu
35 for a fluorenyl group. The η_5 -cyclopentadienyl groups can
be substituted in such a way that they are structurally
attached to each other. Such compounds are known as

bridged metallocenes. It is also possible for the halogen metallocene to contain only one η_5 -cyclopentadienyl group which has a substituent that can coordinate with the metal. Halogen metallocenes which can be used according to the invention are listed under halides in Table 1 on page 7 of EP-A-420,436. Preference is given to halogen metallocenes containing a transition metal chosen from the group comprising Ti, Zr and Hf.

It is preferable to employ a chloride, bromide, iodide or a fluoride as the halide in the halogen metallocene. Specifically, the halogen metallocene is a dihalide, since dihalides exhibit great stability under storage conditions and are easy to prepare. Examples of halogen metallocenes which can be used according to the invention are also given in EP-A-500,944, page 3, line 49 to page 7, line 5.

The co-catalyst of the invention is a compound which can form a stable anion under polymerization conditions. The stable anion is formed through the reaction of the co-catalyst with the reaction product of the halogen metallocene and the alkylating agent. The co-catalyst can be represented by the following general formula:



where Q is the cationic component and Y the anionic component of the co-catalyst which forms the stable anion. m and n are positive integers. The cationic component is chosen for example from the following cations: carbonium, tropylium, ammonium, oxonium, sulphonium, phosphonium, triphenylphosphonium, diphenylcarbonium, cycloheptatrienylium, indenium, triethylammonium, tripropylammonium, tributylammonium, N-N-dimethylanilinium, dipropylammonium, dicyclohexylammonium, triphenylphosphonium, trimethylsulphonium, tris(dimethylphenyl)phosphonium, tris(methylphenyl)phosphonium, triphenylsulfonium, triphenyloxonium,

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triethyloxonium, pyrylium and the cations of silver, gold, platinum, copper, palladium, mercury and ferrocene.

The anionic component Y forms a stable anion when the co-catalyst reacts with the alkylating agent or the reaction product of the halogen metallocene and the alkylating agent. Suitable anionic components are organoboron, organoaluminium, organogallium, organophosphorus, organoarsenic and organoantimony. Examples of such anionic components are tetraphenylboron, tetrakis(3,4,5-trifluorophenyl)boron, tetrakis(3,5-difluorophenyl)boron, tetrakis(3,5-di(t-butyl)-phenyl)-boron, tetrakis(pentafluorophenyl)boron, tetraphenyl-aluminium, tetrakis(3,4,5-trifluorophenyl)aluminium, tetrakis(3,5-di(t-butyl)phenyl)aluminium, tetrakis-(pentafluorophenyl)aluminium, tetraphenylgallium, tetrakis(3,4,5-trifluorophenyl)gallium, tetrakis-(trifluoromethyl)phenyl)gallium, tetrakis(3,5-di(t-butyl)phenyl)gallium, tetrakis(pentafluorophenyl)gallium, tetraphenylphosphorus, tetrakis(pentafluorophenyl)-phosphorus, tetraphenyl arsenic, tetrakis(pentafluorophenyl) arsenic, tetraphenyl antimony, tetrakis(pentafluorophenyl) antimony, decaborate, undecaborate, carbadodecaborate and decachlorodecaborate.

The quantity of co-catalyst used depends on the chosen co-catalyst and can be determined by means of simple experiments. In particular the quantity of co-catalyst is such that the molar ratio of halogen metallocene and co-catalyst is 0.1-10, more specifically 0.5-3.0.

The alkylating agent of the invention is a mixture or reaction product of an alkylaluminium compound and an alcohol. The alcohol can be a monohydric or a polyhydric alcohol. It is preferable to employ a linear or branched C1-C12 alcohol. Particularly suitable as an alkylating agent is the reaction product of trimethyl aluminium, triethyl aluminium or triisobutyl aluminium and methanol or ethanol. In general, the alkylating agent is

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composed in such a way that the OH/Al molar ratio (ratio between the OH-groups in the alcohol and Al) is 0.1-10. Depending of the compounds of the catalyst system used, an optimum is present in the amount of alcohol to be used, relative to the amount of aluminium alkyl. This optimum lies in several cases between an OH/Al ratio of 0.25 and 4.

The quantity of alkylating agent should be such that almost all the halogen metallocene is alkylated. If insufficient alkylating agent is present, the catalyst activity is too low. It is preferable to use such a quantity of alkylating agent that the molar ratio between aluminium and halogen metallocene is greater than or equal to 10, more preferably between 10-50.

The reaction of the halogen metallocene, the alkylating agent and the co-catalyst can take place in different ways. The sequence of addition to the catalyst suspension or the polymerization reactor is generally not critical. Often, the best results are obtained when the co-catalyst is only introduced into the reactor after the other components of the catalyst system. This method for introducing the catalyst components results in increased catalyst activity.

The catalyst of the invention can be used as a catalyst component in the polymerization of olefins in accordance with prior art methods for metallocenes, in particular in the polymerization of olefins chosen from the α -olefins group, internal olefins or diolefins. Mixtures of these can also be employed.

The process of the invention is particularly suitable for polymerizing α -olefins. The α -olefins are preferably chosen from the group comprising ethylene, propylene, butylene, pentene, heptene and octene, the use of mixtures also being possible. It is more preferable to employ ethylene and/or propylene as the α -olefin. The use of such olefins results in the formation of crystalline polyethylene homopolymers and copolymers having both high

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and low density, (HDPE, LDPE, LLDPE, etc.) and polypropylene homopolymers and copolymers (PP and EMPP). The monomers required for such products and the processes to be employed are known to a person skilled in the art.

5 The process of the invention is also suitable for the preparation of amorphous or rubbery copolymers based on ethylene and another α -olefin. It is preferable to use propylene as the other α -olefin, so that EPM-rubber is formed. It is also readily possible to use a diene in
10 addition to ethylene and the other α -olefin, so that a so-called EADM rubber is formed, in particular EPDM (ethylene-propylene-diene rubber).

 The catalysts of the invention can be supported on a carrier or employed without a carrier. Catalysts
15 supported on a carrier are mainly used in gas-phase and slurry processes. The carrier is any carrier which is known as a carrier for metallocene catalysts, for example SiO_2 or Al_2O_3 .

 The catalysts are particularly suitable for use
20 as unsupported catalysts in solution polymerization processes. In solution polymerization the commonly known solvents can be used. It is preferable to use aliphatic hydrocarbons, such as hexane and heptane, and mixtures of aliphatic hydrocarbons.

25 When an aliphatic hydrocarbon is used as a solvent, the solvent can still contain small quantities of aromatic hydrocarbons, for example toluene.

 In the case of the solution polymerization of ethylene or ethylene with other α -olefins and/or non-
30 conjugated dienes up to a comonomer content of 25%, reactor temperatures of at least 130°C are used to keep the produced polymer in solution. With comonomer percentages on a weight basis of 30 - 80 %, the catalysts of the invention supply such a homogeneous product that
35 polymerization can be carried out at much lower reactor temperatures ($\geq 30^\circ\text{C}$) without the formed polymer being precipitated from the solution. Other suitable α -olefins

are, for example, propylene, butylene, hexene and octene.

The olefin can be polymerised in the known way, in both a gas phase and a liquid reaction medium. For the latter, both solution and suspension polymerization can be used.

The process of the invention will be explained hereinafter with reference to the preparation of polyethylene, known from prior art, which is representative of the olefin polymerizations under consideration. For the preparation of other polymers on the basis of an olefin, the reader is expressly referred to the numerous publications on the subject.

The polymerization reaction is generally carried out at a temperature of between -40 and 200°C, preferably between 10 and 180°C. The pressure will generally be 0.1-5 MPa but higher or lower pressures can be used. It is preferable to carry out the process continuously, but it can also be conducted semi-continuously or batchwise.

The residence time can range from a few seconds to a few hours. In general, a residence time of between a few minutes and an hour will be chosen.

The polymerization can be carried out in a liquid which is inert with respect to the catalyst, for example one or more aliphatic saturated hydrocarbons, such as butane, pentane, hexane, heptane, pentamethylheptane or petroleum fractions; aromatic hydrocarbons, for example benzene or toluene, or halogenated aliphatic or aromatic hydrocarbons, for example tetrachloroethylene. It is possible to use such a temperature and pressure that one or more of the monomers employed, in particular the α -olefin, for example propylene, is liquid and present in such a large quantity that it functions as a dispersing medium. In that case, another dispersing medium is unnecessary. The process of the invention can be carried out either in a polymerization reactor filled with gas and liquid or in a reactor completely filled with liquid. By making use of a heterogenized catalyst, it is possible to

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carry out the polymerization process in a suspension or in the gas phase.

The molecular weight can be controlled using techniques known to a person skilled in the art. In particular this can be accomplished by using chain
5 terminating agents, such as diethylzinc, preferably with hydrogen. Even very small quantities of hydrogen influence the molecular weight to a sufficient degree.

After the polymerization, the polymer can be
10 recovered in various ways. Both the evaporation of the solvent and steam coagulation can be used for this purpose in liquid phase processes.

The process of the invention is also suitable for the preparation of amorphous copolymers of olefins.
15 The amorphous copolymers obtained according to the process of the invention generally contain between 25 and 85 wt.-% ethylene. However it is preferable to prepare products with an ethylene content of between 40 and 75 wt.-%.

The invention will be explained hereinafter with
20 reference to the following examples and comparative experiments. The results of the polymerization in the examples are expressed by means of two parameters which have the following meaning:

T jump: temperature rise that occurs in the polymerization
25 reactor during polymerization. This is indicative of catalyst activity.

PE yield: quantity of polyethylene (PE) produced in a specified time (5 minutes). The PE yield is a measure of the catalyst activity.

30

Example I, Synthesis of rac-(1,2-ethylene (bis-(1-Ind)))ZrCl₂

32.7 ml of a 1.6 M solution of butyl lithium in hexane was added to a cooled solution (-56°C) of 6.75 g
35 (26.1 mmol) of 1,2-ethylene(bis-(1-indene)) in 120 ml of diethylether in a Schlenk flask. The precipitate formed was filtered off and washed with 120 ml of hexane,

- 10 -

suspended in 80 ml of dimethoxyethane and cooled to -20°C. After cooling to -56°C, the suspension was added to a suspension of 5.78 g zirconium tetrachloride, cooled to -56°C, in 40 ml of dimethoxyethane. After some time, a yellow precipitate was formed, which was filtered off and vacuum dried. The yield was 65% rac-(1,2-ethylene(bis-(1-indenyl))) zirconium dichloride.

Example I

10 Polymerization of ethylene

A 1.3 litre autoclave was filled with 450 ml of pentamethylheptane. The reactor was pressurized to 2 MPa by introducing ethylene and the reactor contents were preheated to 165°C. 5 ml of toluene, 5 ml of a 0.04 M solution of an aluminium alkyl compound in gasoline and 1 ml of a 0.2 M alcohol solution in gasoline were successively introduced into a tank. The molar ratios are given in Table 1. After stirring for 1 minute, 1 ml of a 0.01 M slurry of the rac-1,2-ethylene(bis-(1-indenyl)) zirconium dichloride in gasoline, obtained as described above, was added. After stirring for a minute, a [DMAH][BF₂O](dimethylanilinium tetrakis(pentafluorophenyl) boron) slurry in gasoline was added. After stirring for another minute, the catalyst mixture obtained in this way was dosed to the reactor at 165°C with 50 ml of pentamethylheptane. During the polymerization the temperature in the reactor rose. After 5 minutes the polyethylene solution was drained off and the product was worked up and dried. For the results see Table 1.

30

Comparative experiment A

The polymerization was carried out as in Example I, using the same catalyst, but without the addition of the alcohol. No polymerization activity was observed.

35

Examples II and III

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The procedures followed were analogous to that of Example I, but the amount of alcohol was changed such that the molar quantities of alcohol with respect to aluminium in the alkylating agent were 2 and 0.5

5 respectively instead of 1. As can be seen from the results of Examples I-III, an optimum in the Alcohol/Aluminium ratio is present.

Example IV

10 The catalyst and the polymerization were as in Example I, but the alcohol employed was 2-ethyl-1-hexanol instead of methanol. See Table 1.

15 Table 1 : Polymerization of ethylene in the presence of a catalyst system from rac-(1,2-ethylene(1-Ind)₂)ZrCl₂, [DMAH][BF₂O], trimethylaluminium (TMA) and alcohol; ratio [DMAH][BF₂O]/Zr= 2, Al/Zr= 20.

20

Example/ experiment	Alcohol type	Molar ratio Alcohol/Al	T-rise (°C)	PE yield (g)
I	methanol	1	43	15
A	-	-	0	0
25 II	methanol	2	0	0
III	methanol	0.5	17	4
IV	2-ethyl-1- hexanol	1	47	16

Example VSynthesis of 1,2-ethylene(Cp)(2-Ind)ZrCl₂

The synthesis of ethylene(Cp)(2-Ind)ZrCl₂ was carried out in accordance with steps V.1 - V.4 described below.

V.1 Synthesis of ethyl(2-indene)acetate

At 15°C, a solution of 31.3 g of triethylphosphonoacetate in 75 ml of THF was evenly metered over a period of 1 hour 15 minutes into a suspension of 3.30 g of sodium hydride in 200 ml of tetrahydrofuran (THF). The mixture was then stirred for a further 30 minutes at room temperature. A solution of 18.1 g of 2-indanone in 75 ml of THF was metered into this mixture over a period of 1 hour with cooling using a water bath. The mixture was then stirred for 45 minutes at room temperature. Working-up: the reaction mixture was poured into water, the water and reaction mixture were subjected to an extraction process, using diethylether, the ether layer was dried on a bed of magnesium sulphate and the resulting mixture was then filtered and the filtrate evaporated. The yield was 27.4 g of crude reaction product. After distillation under vacuum, 22.4 g (80%) of ethyl(2-indene)acetate was obtained.

V.2 Synthesis of 2(2-indene)ethanol

At room temperature, a solution of 7.0 g of ethyl(2-indene) acetate in 50 ml of diethylether was added dropwise to a suspension of 1.41 g of lithium aluminium hydride in 100 ml of diethylether. The temperature rose to 30°C; the total dosing time was 60 minutes. The mixture was stirred for 30 minutes at room temperature. Next 25 ml of water was added and the mixture was stirred for 15 minutes. After the mixture was poured into ice and concentrated sulphuric acid was added, the product was worked up. The product was purified over a silica column (mobile phase: hexane). The yield was: 4.0 g of pure

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2(2-indene)ethanol (72 %).

V.3.Synthesis of 1-bromo-2(2-indene)ethane

11.8 g of triphenylphosphine was added to a
5 solution of 7.1 g of 2(2-indene)ethanol in 100 ml of THF
and 8.0 g of N-bromosuccinimide was subsequently added in
small amounts at room temperature. The total dosing time
was 1 hour. Stirring was then continued for 30 minutes at
room temperature. The reaction mixture was poured out into
10 300 ml of hexane and the formed precipitate was filtered
off and washed twice with 50 ml of hexane. The combined
hexane fractions were evaporated and the product was
purified over a silica column (mobile phase:hexane). The
yield was: 7.9 g of 1-bromo-2(2-indene)ethane (80%).

15

V.4.Synthesis of 1-cyclopentadiene-2(2-indene)ethane

At -35°C, a solution of 18.2 g of 1-bromo-2(2-
indene)ethane in 100 ml of THF was added over a period of
two hours to a solution of 120 mmol cyclopentadiene sodium
20 (NaCp) in 260 ml THF. Stirring was then carried out for a
further 30 minutes at this low temperature and
subsequently for 16 hours at room temperature. After the
addition of water, the evaporation of THF, extraction
using diethylether, the drying of the organic layers and
25 the evaporation of the solvent, the product was purified
over silica (mobile phase: petroleum ether boiling range
40-60°C). Yield: 7.1 g of (41 %) 1-cyclopentadiene-2(2-
indene)ethane.

V.5.Synthesis of 1,2-ethylene (1-cyclopentadienyl) (2- indenyl)zirconium dichloride

The synthesis of the metallocene compound was
carried out as in Example I, but in this case with:
2.94 g of 1-cyclopentadiene-2(2-indene)ethane,
35 17.6 ml of 1,6 M n-butyllithium (BuLi) in hexane,
and 3.2 g of zirconium tetrachloride.

5.05 g of solid light-yellow compound, 1,2-

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ethylene(Cp)(2-Ind)ZrCl₂, was obtained. A portion of the product was freed from lithium chloride by extraction using dichloromethane. Taking into account 2 equivalents LiCl the yield of crude product was 83%. Extraction of
5 2.05 g of crude product (containing LiCl) with 100 ml of CH₂Cl₂ gave 1.3 g of pure product.

1H NMR in CDCl₃ : 7.5 (m, 2H, of Cp), 7.2 (m, 2H, of Cp), 6.5 (t, 2H, C6 of Ind), 6.2 (s, 2H, C5 of Ind), 6.1 (t, 2H, C6 of Ind), 3.15 (s, 4H, of ethylene)
10

Example V

Polymerization

The polymerization was carried out as in Example I, but with 1,2-ethylene(Cp)(2-Ind)ZrCl₂,
15 triethylaluminium (TEA) and 2-ethyl-1-hexanol as elements of the catalyst system. The metallocene concentration in the reactor was 0.02 mM. The molar ratio alcohol/Al was 1/10. The results are given in Table 2.

Comparative experiment B

As Example V, but without 2-ethyl-1-hexanol. The results are given in Table 2.

Examples VI and VII

25 As Example V, but with different amounts of 2-ethyl-1-hexanol. See Table 2.

Example VIII

30 As example VII, but with trimethylaluminium (TMA) as the co-catalyst.

Comparative experiment C

As Example VIII, but without using alcohol. This gave a very low activity (see Table 2).
35

Examples IX-XI

In these examples TEA and pentaerythritol

- 15 -

(C(CH₂OH)₄, 0.2 M slurry in gasoline) were used in different molar ratios of alcohol and aluminium. See Table 2. The activity is lower than when 2-ethyl-1-hexanol is used.

5

Table 2: Polymerization of ethylene in the presence of the catalyst 1,2-ethylene(Cp)(2-Ind)ZrCl₂, [DMAH][BF₂O], aluminium alkyl (trimethyl-aluminium (TMA) or triethylaluminium (TEA)) and alcohol;

10

ratio [DMAH][BF₂O]/[Zr] = 2, [Al]/[Zr] = 20.

15

20

Ex.	Aluminium alkyl type	Alcohol type	Molar ratio Alcohol/Al	Molar ratio OH/Al	T-jump (°C)	PE yield (g)
V	TEA	2-ethyl-1-hexanol	0.1	0,1	32	11
B	TEA	-	-	-	26	10
VI	TEA	2-ethyl-1-hexanol	0.5	0,5	45	14
VII	TEA	2-ethyl-1-hexanol	1	1	65	39
VIII	TMA	2-ethyl-1-hexanol	1	1	62	33
C	TMA	-	-	-	14	2
IX	TEA	penta-ery-thritol	0.25	1	34	8
X	TEA	penta-ery-thritol	0.5	2	42	16
XI	TEA	penta-ery-thritol	1	4	15	2

Example XIIPolymerization of ethylene at lower reactor temperature

The catalyst as prepared in Example V was used for the polymerization of ethylene at a reactor temperature of 50°C. The reactor was a 1.5 litre autoclave, the dispersing medium was 500 ml of gasoline. The reactor was filled with ethylene to an ethylene pressure of 0.7 MPA. Triethylaluminium in a concentration of $4 \cdot 10^{-4}$ mol/l was added to the dispersing medium to render impurities in the reactor harmless ("scavenger"). In a catalyst preparation vessel, aluminium alkyl, alcohol, metallocene compound and co-catalyst were successively premixed in a molar ratio of 20:20:1:3. The catalyst mixture was subsequently introduced into the reactor. The concentration of metallocene compound in the reactor was $5 \cdot 10^{-6}$ mol/l. The concentration of co-catalyst ([DMAH][BF₂O]) was $1.5 \cdot 10^{-5}$ mol/l. After a polymerization time of 9 minutes the polymer was recovered, treated with methanol and vacuum dried at 60°C. For the results see Table 4.

Example XIII and Comparative Experiment E

This example and the comparative experiment were carried out as Example XII, with the aluminium alkyl compound and alcohol indicated in Table 4. For the results see Table 4. When no alcohol is added hardly any polymerization activity is observed.

Table 4 : Polymerization of ethylene at 50°C in the presence of 1,2-ethylene (Cp)(2-Ind)ZrCl₂ catalyst

5

Ex.	Aluminium alkyl type	Alcohol type	Catalyst activity (kgPE/gZr*5 min)
XII	TEA	2-ethyl-1-hexanol	15
X	TEA	-	3
XIII	TMA	2-ethyl-1-hexanol	16

- 10 It has been found experimentally that both the co-catalyst and the alkylating agent are essential for achieving sufficiently high catalyst activity in the polymerization of olefins. When adding the co-catalyst, alkylating agent and halogen metallocene to the reactor, it is preferable
- 15 to employ a sequence such that the alkylating agent and the co-catalyst are not brought into contact first.

C L A I M S

1. Process for the polymerization of an olefin in the presence of a catalyst system comprising:
 - 5 a) a halogen metallocene
 - b) a co-catalyst which forms a stable anion
 - c) an aluminium-containing alkylating agent, characterised in that the aluminium-containing alkylating agent is a mixture or reaction product of
- 10 2. Process according to claim 1, characterised in that the alkyl aluminium compound is chosen from trimethylaluminium, triethylaluminium or triisobutylaluminium.
- 15 3. Process according to any of claims 1-2, characterised in that the quantity of co-catalyst is such that the halogen metallocene/co-catalyst molar ratio is 0.1-10.
- 20 4. Process according to claim 3, characterised in that the quantity of co-catalyst is such that the halogen metallocene/co-catalyst molar ratio is 0.5-3.0.
5. Process according to any of claims 1-4 characterised in that the quantity of alkylating agent is such that the Al/halogen metallocene ratio is greater than or
- 25 equal to 10.
6. Process according to claim 5, characterised in that the Al/halogen metallocene ratio is 10-50.
7. Process according to any of claims 1-6, characterised in that the alkylating agent comprises an alcohol
- 30 with 1-12 C-atoms.
8. Process according to any of the claims 1-7 characterised in that the halogen metallocene contains a transition metal, chosen from the group comprising Ti, Zr and Hf.
- 35 9. Polyolefin obtainable according to the process of any of the claims 1-8.

10. Catalyst system suitable for the polymerization of an olefin comprising:
- a) a halogen metallocene
 - b) a co-catalyst which forms a stable anion
 - 5 c) an aluminium-containing alkylating agent, characterised in that the aluminium-containing alkylating agent is a mixture or reaction product of an alkyl aluminium compound and an alcohol.

INTERNATIONAL SEARCH REPORT

International Application No
PS/NL 94/00242A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 C08F10/00 C08F4/605

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 6 C08F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP,A,0 513 380 (IDEMITSU KOSAN COMPANY) 19 November 1992 see examples 7-9,27-31 see claims 1,2 see page 10, line 13 - line 16 ---	1
A	EP,A,0 500 944 (MITSUI TOATSU CHEMICALS) 2 September 1992 see claim 1 see example 1 --- -/--	1

☒ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

* Special categories of cited documents :

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Date of the actual completion of the international search

20 January 1995

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Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
Fax (+31-70) 340-3016

Authorized officer

Fischer, B

INTERNATIONAL SEARCH REPORT

International Application No
PCT/NL 94/00242

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	<p>DIE MAKROMOLEKULARE CHEMIE, RAPID COMMUNICATIONS, vol.14, no.2, February 1993 pages 109 - 114, XP334497 JAMES C.W. CHIEN 'Olefin copolymerization and olefin/diene terpolymerization with a zirconium catalyst system' see page 110</p> <p>-----</p>	1

Form PCT/ISA/210 (continuation of second sheet) (July 1992)

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No.

PCT/NL 94/00242

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